

Rules of Thumb

Facts about compressed air and compressed air systems.

LEAK FLOW RATES								
Based on flow through an orifice.								
Upstream Psig	Orifice Diameter (Inches)				Orifice Diameter (Inches)			
	1/16"	1/8"	1/4"	1/2"	1/16"	1/8"	1/4"	1/2"
	Discharge, cfm Free Air				Annual Cost			
80	5	21	85	340	\$757	\$3,028	\$12,111	\$48,443
100	6	26	103	411	\$917	\$3,669	\$14,674	\$58,696
120	8	30	121	483	\$1,077	\$4,309	\$17,237	\$68,949
*Based on air temperature of 60° F.					*Based on 4 CFM/HP and 8¢/kWH			

PIPE SIZING MAX. RECOMMENDED CFM								
Based on 0.5 psi drop per 100' of pipe.								
PSIG	3/4"	1"	1 1/2"	2"	2 1/2"	3"	4"	6"
80	20	40	125	225	375	675	1350	4000
100	22	42	135	250	410	740	1510	4450
125	25	45	145	280	450	810	1640	4900

The flow contribution from a storage tank can be estimated as follows:

$$\text{Flow from tank (cfm)} = \frac{\text{Volume} \times (P_1 - P_2)}{\text{Time} \times P_0}$$

Where:

- Volume = Volume of the tank in Cubic Feet
- P₁ = Starting pressure inside the tank (psig)
- P₂ = Ending pressure inside the tank (psig)
- Time = Time of the pressure drop event (minutes)
- P₀ = Atmospheric pressure (usually 14.7 psia)

7.4805 gallons per Cubic Foot
 0.1337 Cubic Feet per Gallon

Metric Conversions
 cfm = lpm X 0.0353
 lps = cfm X 0.472
 1 bar = 14.5 psi
 kg/cm² = 14.22 psi

$$\text{kW} = \frac{0.746 \times \text{bHP}}{\text{Motor Efficiency}}$$

Effect of stabilizing Plant Pressure with FlowLogic Controller.

$$\text{Net flow} = \text{Current flow} \times \frac{\text{New Set Pressure (psia)}}{\text{Current Average Pressure (psia)}}$$

Rule of Thumb Annual Cost
 Energy Cost (\$) = HP × 550
 (Assuming 8760 Hours/year at 8¢/kWH)

$$\text{Energy Cost (\$)} = \text{kW} \times \text{Operating Hours} \times \text{\$/kWH} \times \text{AVG. \% loaded} + \text{kW (max.)} \times \text{Demand Charge}$$

$\text{kW (3 Phase)} = \frac{\text{Amps} \times \text{Volts} \times 1.73 \times \text{Power Factor}}{1000}$	$\text{BHP (3 Phase)} = \frac{\text{Amps} \times \text{Volts} \times 1.73 \times \text{Power Factor} \times \text{Motor Efficiency}}{746}$
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Purge Rate for Regenerative Dryers: Heatless 15% / Heated 7% / Blower Purge 3%

Rule of thumb formulas for single stage rotary screw air compressor systems:

$\text{Power Change} = \frac{5\% \text{ Increase in Power}}{10 \text{ Psig Increase in Pressure}}$	$\text{Capacity Change} = \frac{0.75\% \text{ Increase in Capacity}}{10 \text{ Psig Decrease in Pressure}}$
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1 Hp ≈ 4 to 5 cfm Cost to run a compressor ≥ \$1.25 per HP per Day

- A 100 cfm compressor (25 Hp), ingests approximately 18 gallons of water per day on a 75°F, 75% RH day.
- A properly operating after cooler and separator will remove approximately 68% of the water ingested by the compressor.
- A properly operating refrigerated dryer and drain will remove 28% of the ingested water leaving approximately 4.0%.
- A properly operating desiccant dryer will remove 32% of the ingested water, leaving approximately 0.3%.

